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In the claims:

Please amend the claims as shown below:

- 5 1. (Currently amended) A method for the dilution of  
dewatered and compressed cellulose pulp that has been  
consolidated into large pieces, where the dewatered  
cellulose pulp maintains a first consistency greater than  
20%, ~~preferably greater than 25%, and even more preferably~~  
10 ~~greater than 30%, whereby comprising:~~  
~~fragmenting the cellulose pulp is fragmented~~ into a finely  
divided pulp after or in association with dewatering, ~~c h a r~~  
~~a c t e r i s e d i n~~  
~~granulating that the cellulose pulp is granulated~~ through  
15 fragmentation to a particle size with a normal distribution  
with a maximum size that is less than 40 mm, ~~preferably less~~  
~~than 30 mm, and even more preferably less than 20 mm, and~~  
~~that during fragmentation maintains~~  
~~while fragmenting, maintaining a consistency of the cellulose~~  
20 ~~pulp that is essentially equivalent to the first consistency,~~  
~~feeding that the cellulose pulp that has been finely divided~~  
through the fragmentation ~~is fed out~~ into a freely falling  
flow,  
~~adding that~~ dilution fluid ~~is added~~ under pressure towards  
25 the freely falling fragmented pulp through a number of fluid  
jets (62) arranged in association with the flow of the freely  
falling fragmented pulp,  
~~that~~ the amount of dilution fluid added through the said  
fluid jets (62) ~~establishes~~ establishing a second consistency  
30 of the cellulose pulp in ~~the~~ a medium-consistency range 8-  
16%,  
~~feeding that the cellulose pulp at this medium consistency 8-~~

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16% ~~is fed onwards~~ onwardly to subsequent treatment stages,  
that the a dilution of the freely falling pulp ~~down to a~~  
~~medium consistency of 8-16% before it the freely falling pulp~~  
~~is fed onwards onwardly to subsequent treatment stages takes~~  
5 taking place essentially exclusively under ~~the~~ an influence  
of hydrodynamic effect from the addition of the dilution fluid  
through the ~~said~~ fluid jets, and where no mechanical  
agitation ~~takes taking~~ place between the fragmentation of the  
cellulose pulp and ~~the~~ an underlying surface (Liq<sub>LEV</sub>) of the  
10 cellulose pulp that has been diluted by the dilution fluid  
~~that has been established.~~

2. (Currently amended) The method according to claim 1, ~~ch~~  
~~aracterised in that~~ wherein the fluid jets  
15 are arranged around the flow of fragmented pulp formed in  
the free fall, and are directed principally radially  
inwards towards the flow.

3. (Currently amended) The method according to claim 1, ~~ch~~  
20 ~~aracterised in that~~ wherein the cellulose  
pulp at medium consistency is fed ~~onwards~~ onwardly to  
subsequent treatment stages through pumping.

4. (Currently amended) The method according to ~~either claim~~  
25 ~~1 or claim 2, characterised in that~~ claim 1  
wherein the dilution fluid added is added to a degree of  
more than 50%, ~~preferably more than 75-90%~~, through the  
~~said~~ fluid jets ~~(62)~~.

30 5. (Currently amended) The method according to ~~any one of~~  
~~claims 1-3, characterised in that~~ claim 1  
wherein the addition of dilution fluid from the ~~relevant~~  
fluid jets ~~(62)~~ takes place in ~~the~~ a form of pressurized

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~~pressurised~~ fluid jets that are directed obliquely  
~~downwards~~ downwardly in ~~the~~ a fall direction ~~of fall~~ of  
the cellulose pulp.

- 5 6. (Currently amended) The method according to claim 4, ~~ch~~  
~~a-r-a-c-t-e-r-i-s-e-d~~ ~~i-n~~ that wherein the fluid jets  
are directed at an angle of  $45^{\circ} \pm 15^{\circ}$  relative to ~~the~~ a  
vertical direction and ~~the~~ a fall direction ~~of fall~~ of the  
granulate.

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7. (Currently amended) A device for the dilution of  
dewatered cellulose pulp, comprising:  
shredder screw means for fragmenting pulp to a particle size  
in an interval of 5-40 millimeters, the shredder screw means  
15 having an outlet defined therein, the shredder screw means  
containing the fragmented pulp,  
a vertical standpipe connected to the outlet of the shredder  
screw means, the standpipe carrying a flow of the fragmented  
pulp flowing under free fall, the standpipe having a  
20 distribution chamber defined therein at an upper end of the  
stand pipe, the distribution chamber arranged concentrically  
around the standpipe,  
at least four nozzles arranged around a circumference of the  
distribution chamber, the nozzles being oriented inwardly  
25 towards a center of the flow to add a dilution fluid under  
pressure into the stand pipe, the nozzles being disposed above  
a liquid level of diluted pulp established in the standpipe,  
a feed arrangement disposed at a bottom of the standpipe for

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feeding the pulp to subsequent treatment stages,  
a pump disposed at the bottom of the standpipe and in  
operative engagement with the feed arrangement, and  
the standpipe having no mechanical agitator disposed above the  
5 liquid level.

~~dewatering equipment (7, 80) to which pulp at an initial~~  
~~consistency in the range 4-12% has been fed and in which the~~  
~~cellulose pulp after dewatering maintains a consistency~~  
~~greater than 20%, preferably greater than 25%, and even more~~  
10 ~~preferably greater than 30%, whereby the cellulose pulp is~~  
~~fed to fragmentation equipment (8, 8b) to be fragmented into~~  
~~a finely divided pulp, characterised in~~  
~~that the cellulose pulp is granulated through fragmentation~~  
~~in the fragmentation equipment (8, 8b) into a particle size~~  
15 ~~with a normal distribution with a maximum size that is less~~  
~~than 40 mm, preferably less than 30 mm, and even more~~  
~~preferably less than 20 mm,~~  
~~that the pulp that has been finely divided is fed from the~~  
~~outlet of the fragmentation equipment into an essentially~~  
20 ~~vertical stand pipe (22/40'), under free fall,~~  
~~that a number of nozzles (62) are arranged around the~~  
~~circumference of the stand pipe (22), from which nozzles~~  
~~dilution fluid (LiqDIL) is added under pressure into the~~  
~~stand pipe and above a level (LiqLEV) of diluted cellulose~~  
25 ~~pulp established in the stand pipe,~~  
~~where the amount of added dilution fluid (LiqDIL) establishes~~

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~~a consistency of the cellulose pulp in the range of medium consistency 8-16% and that this added amount, to more 50%, preferably to more than 75-90%, is added through the said nozzles (62) arranged above a level (LiqLEV) established in the stand pipe,~~

~~that the cellulose pulp at this medium consistency is fed onwards to subsequent treatment stages by a feed arrangement (41),~~

~~that the dilution of the pulp to a medium consistency of 8-16% in the stand pipe takes place exclusively under the influence of hydrodynamic effect from the addition of dilution fluid through the said nozzles and without the use of a mechanical agitator above the level (LiqLEV) of fluid established in the stand pipe (22/40').~~

8. (Currently amended) The device according to claim 7 ~~characterised in that~~ wherein the device has the cellulose pulp at this medium consistency is fed onwards to subsequent treatment stages for the cellulose pulp with a the pump (41) connected to the stand pipe ~~(22/40')~~ at its a lower part thereof close to the bottom of the stand pipe, under the liquid level ~~(LiqLEV)~~ of fluid established.

9. (Currently amended) The device according to claim 7 ~~characterised in that~~ wherein the nozzles at least four nozzles are arranged around a periphery of the stand pipe, where a distance between neighbouring nozzles is less than 50-300 mm ~~(22/40')~~.

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10. (Currently amended) The device according to claim 9 ~~is~~  
~~characterised in that wherein~~ each nozzle is  
directed ~~in towards the centre of the stand pipe and~~  
5 ~~obliquely downwards~~ at an angle relative to the vertical  
~~and the~~ a direction of free fall of the fragmented pulp  
granulate of  $45 \pm 15^\circ$ .
11. (Currently amended) The device according to claim 10 ~~is~~  
10 ~~characterised in that wherein~~ all nozzles are  
connected to a common distribution chamber ~~(60)~~ for  
dilution fluid, ~~which the~~ chamber is ~~pressurised~~  
pressurized through a pressure-raising device ~~(61)~~.
12. (New) The device according to claim 7 wherein the  
15 nozzles are oriented obliquely downwardly.

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